

Energy Efficient Ultra-low NOx Burner (ULNB) Control Technology

**Food Industry Energy Research
(FIER) RD&D Project Review
University of California, Davis
October 26, 2004**

Project Objective and Need

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- **Project Objective**
 - Reduce Ultra-low NOx Burner (ULNB) Power Consumption by 25%
- **Project Need**
 - Severe ozone non-attainment in San Joaquin Valley
 - New AQMD rule requires boiler retrofits to 9 ppm NOx starting in 2005
 - Significant hardware and operating costs to achieve 9 ppm affect food processors

ALZETA Products

***DURATHERM™
OEM Residential/Commercial Low NO_x Burners***

***CSB™ & CSB microSTAR™
Industrial/Commercial Ultra-Low NO_x Burners***

***EDGE™
Catalytic and Thermal Oxidizers***

CSB™ Ultra-Low NO_x Burners

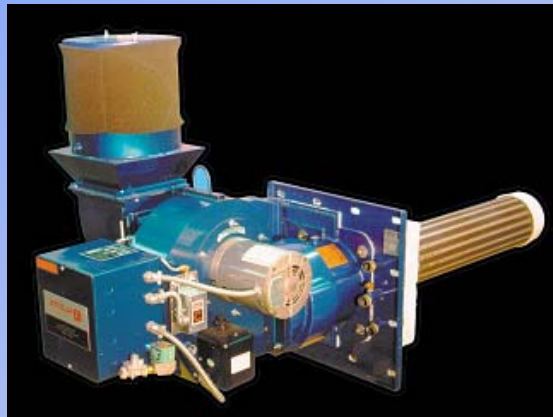
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CSB microSTAR™

**Commercial Boilers
and Process Heaters**

2 – 14.7 MMBtu/hr

0.5 – 4 MW_t



CSB™

**Industrial Boilers
and Process Heaters**

16.8 - 130 MMBtu/hr

4 – 35 MW_t



CSB Product Description

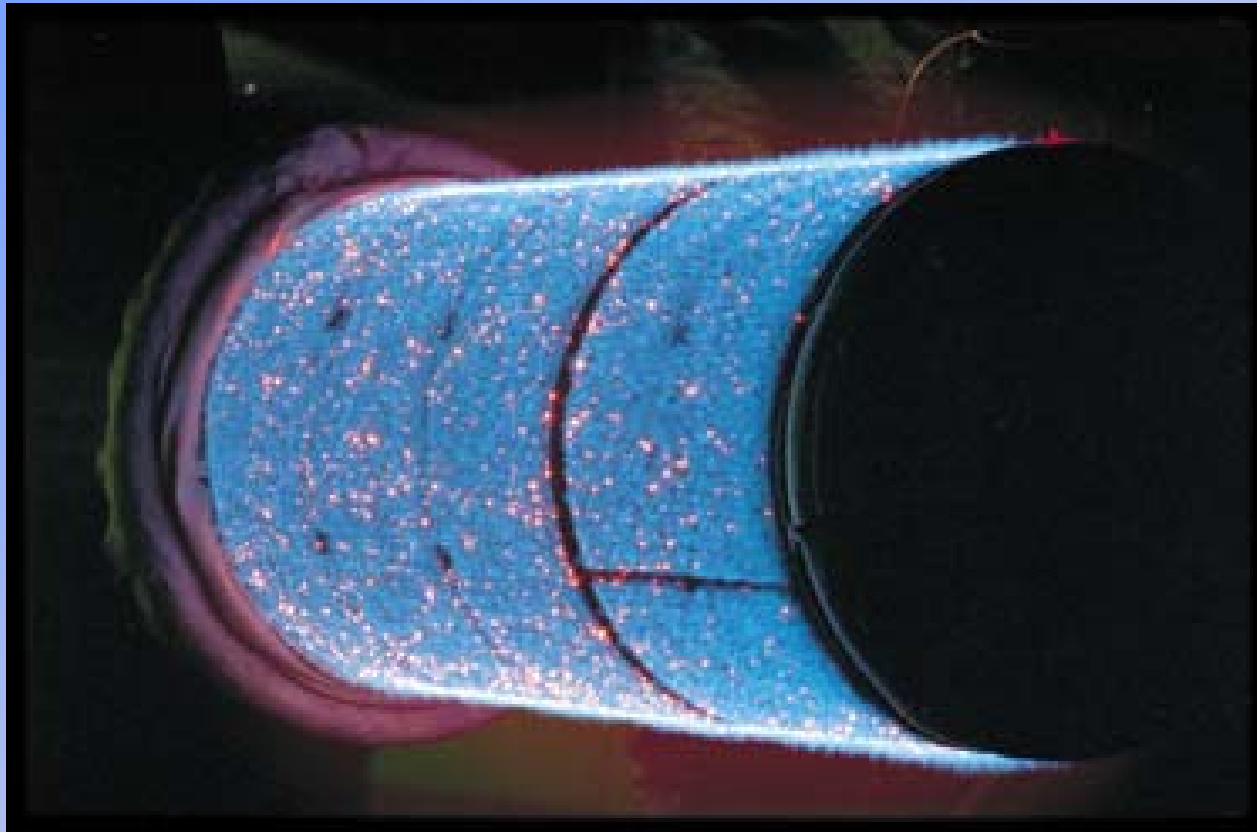
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- Fully Premixed Surface-Stabilized Burner
- All-Metal Burner Surface
- Surface Flux to 1.4 MMBtu/hr/ft²
- Single Burners to 180 MMBtu/hr
- Optimized for Ultra-Low NO_x and CO Emissions

CSB Burner Head

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How the CSB Works

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- **Premixed Combustion**
 - Combustion takes place at uniform temperature
 - Flame temperature a balance between emissions and flame stability
- **Surface Stabilization**
 - Increases flame stability at lean limit
 - Increases heat transfer from flame zone

How Do We Control NO_x?

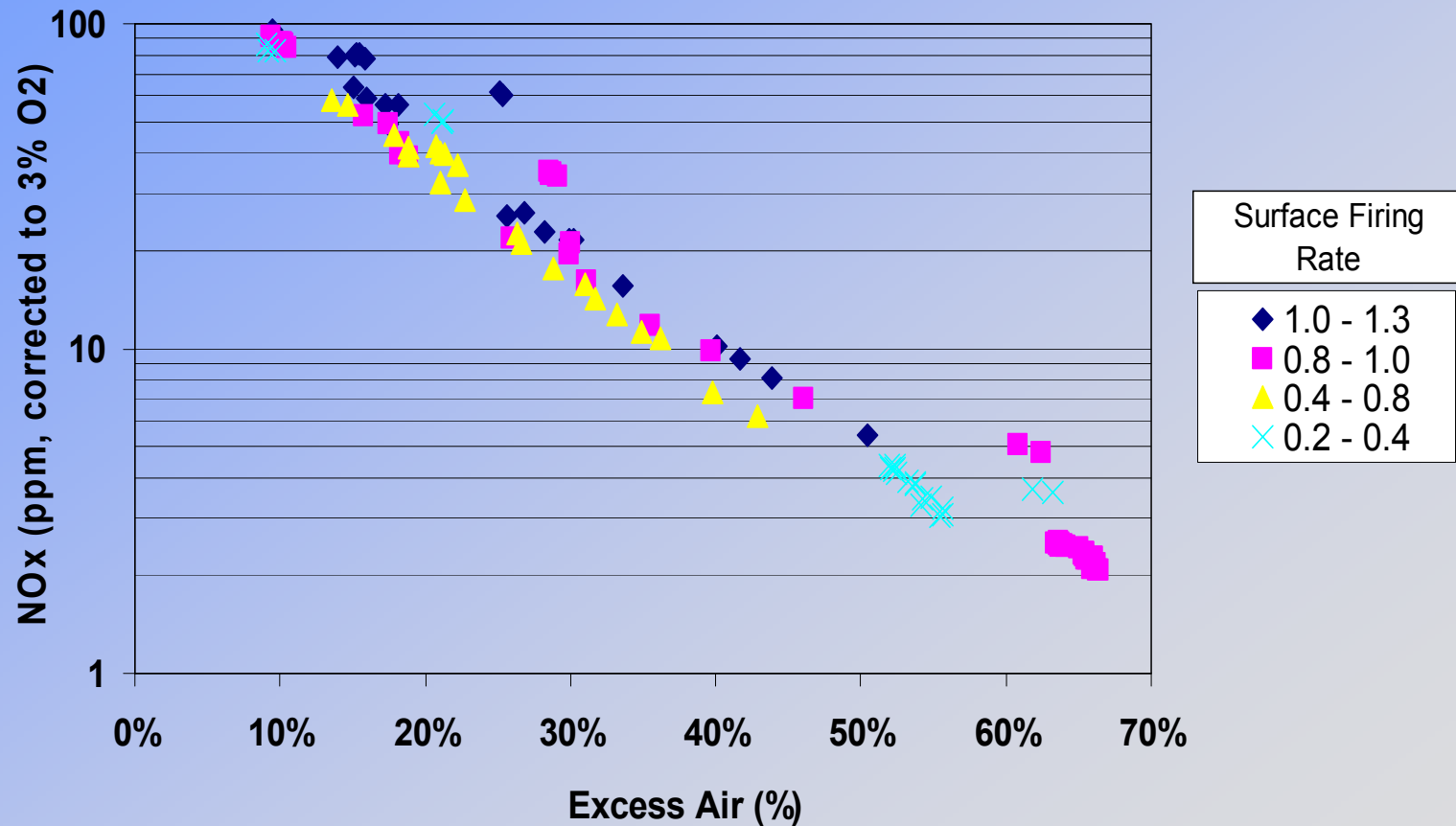
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- NO_x is Primarily a Function of Flame Temperature
 - Flame temperature controlled by dilution of fuel-air premix with additional air or flue gas
 - Heat release rate and furnace design are secondary effects with CSB

CSB NO_x vs Excess Air

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High Efficiency CSB

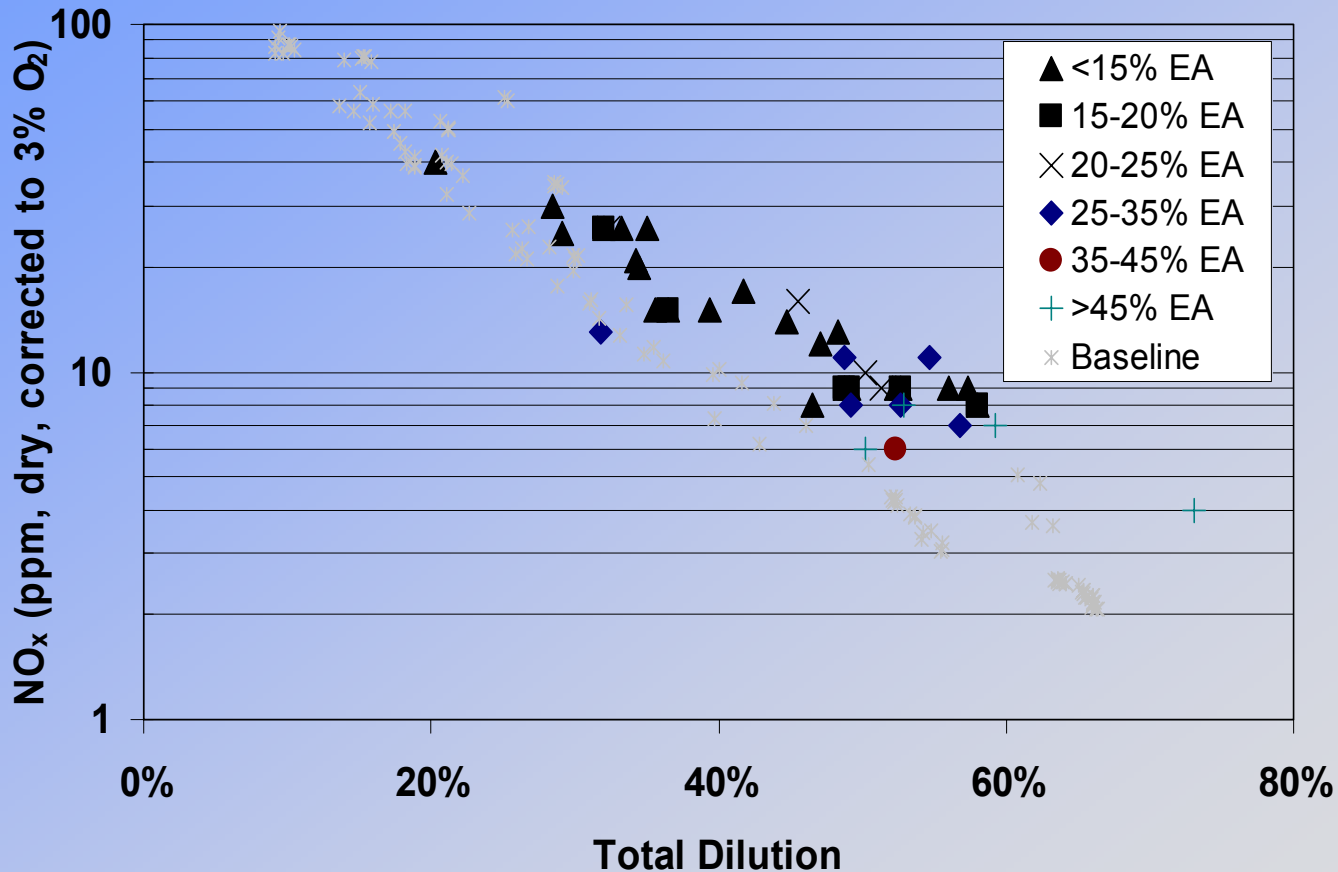
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- **NO_x Reduction with Low Excess Air**
 - Flue Gas Instead of Excess Air Reduces Flame Temperature
 - Lower Flame Temperature = Lower NO_x
- **Flue Gas Recirculation (FGR)**
Reduces Thermal Loss From Stack
 - Low Thermal Loss = High Efficiency

CSB NO_x vs Total Dilution

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Burner and Fan Performance

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- **Burner Behaves as a Constant Mass Flow Device. Heat Input Proportional to Mass Flow of Air**
- **Fan Behaves as Constant Volume Device**
 - For Fixed Density, Power Scales with Mass Flow Cubed! ($dp \times Q$). Dilution requires more power.
 - Lower Density Air Requires Larger Housing and More Work for Fixed Mass Flow

Fan Power Issues

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- Final 20% of Heat Input Requires 50% of Fan Power, Bigger Motors Use More Power at All Load Levels
- FGR Reduces Fuel Usage (Good)
 - Increases Mass Flow and Average Temperature of Diluent Through Fan
 - Therefore INCREASES Fan Size and Power Usage (Bad)

Improving Performance

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- **Fuel Component of Costs is Much Greater Than Electric Component**
 - Doubling Fan Power has Approximate Cost of 1% Decrease in Thermal Efficiency
 - End Users Have Been Willing to Use More Power to Maintain Efficiency
 - But, Improvements Can Be Made!

Relative Fan Requirements

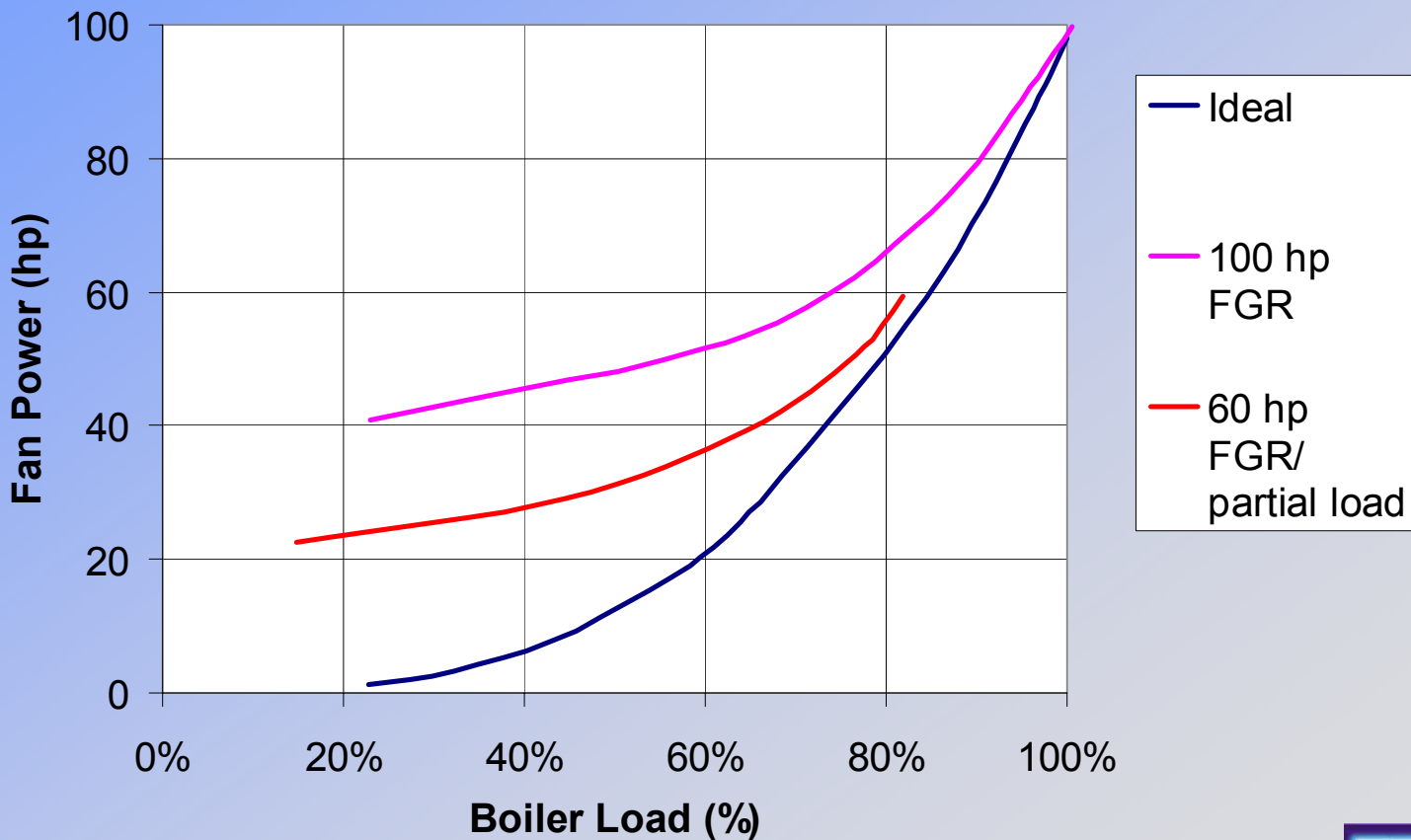
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NO_x Level (ppm)	Relative Mass Flow	Relative Volume (Inverse of Density)	Relative Fan Power	Fan hp for 50 MMBtu/hr Burner
100	1.0	1.0	1	25
30	1.15	1.09	1.80	45
9 (w/Ex.Air)	1.4	1.0	2.74	68
9 (w/ FGR)	1.4	1.22	4.08	102

Fan Power vs Load

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Improving Performance

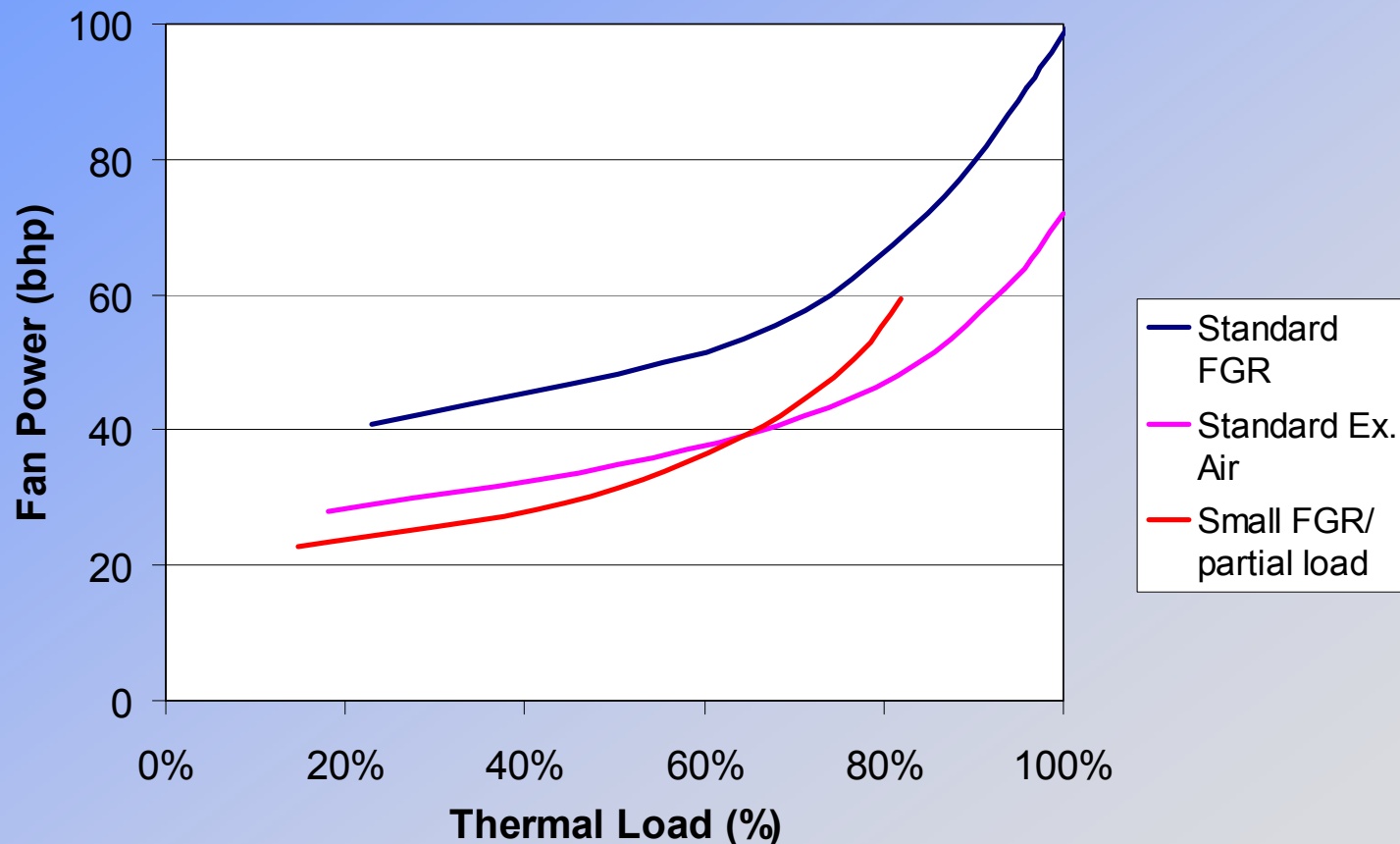
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- **Fan Power Requirement Can be Reduced with Minimal Impact on Thermal Efficiency**
 - Address Power Usage at Top 20% of Thermal Load Curve
 - Maintain Maximum Power Rating while Allowing Thermal Efficiency to Decrease at Maximum Input

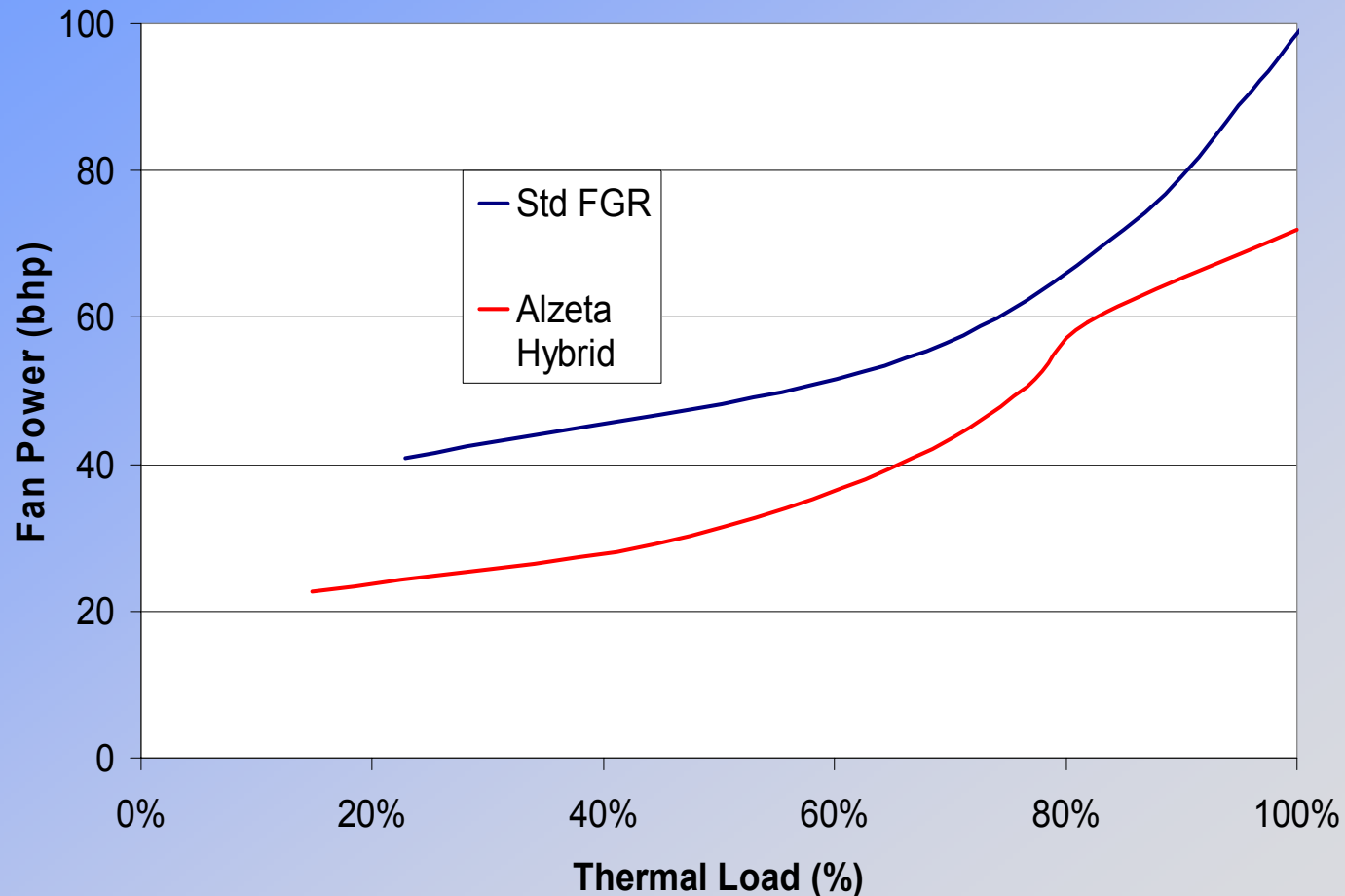
Fan Power w/ EA and FGR

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Current Approach vs Hybrid

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Implementation of Design

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- **Select Fan Housing and Motor for Excess Air Operation at High Fire**
- **Operate at Maximum FGR until “FGR Capacity” reached (~85% load)**
- **From 85-100% Load, Decrease FGR Fraction of Diluent, Increase Mass Flow**

Implementation of Design

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- **Requires fuel-air ratio control modifications**
 - Fixed fan-damper setting with variable fuel input
 - Control modification demonstrated prior to project start
 - Initially developed to track ambient air variation

End User Benefits

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Basis	Annual Operating Cost Savings (\$.10/kWh and 25% average boiler usage)	Capital Cost Savings (25% lower cost of Alzeta fan)
Single User (50 MMBtu/hr burner)	\$4,080	\$3,000
San Joaquin Valley (SJVUAPCD Inv.)	\$6,500,000	\$4,800,000
State of California (Based on ARB Emissions Inventory)	\$21,300,000	\$16,000,000

Reduction in Power Use

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Basis	Reduction in Peak Demand	Reduction in Annual Energy Usage
Single User (50 MMBtu/hr capacity)	18.6 kW	340.8 MW-hrs
San Joaquin Valley (SJVUAPCD Inventory)	29.7 MW	65,300 MW-hrs
State of California (Based on ARB Emissions Inventory)	99.3 MW	217,400 MW-hrs

Summary of Benefits

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- **Reduced Initial Hardware Cost
(Smaller Fan and Lower Amperage
Power Hardware)**
- **Reduced Fan Power at All Load
Levels. Power Savings at All Loads**
- **Increased Thermal Turndown**

Package Watertube Boiler

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Industrial Firetube Boiler

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Demonstration Site

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- **75 MMBtu/hr Package Watertube Boiler**
 - Dairy Products Company Located in Central Valley
 - Installation in Progress for November Startup

Contact Information

Advanced Combustion Clean Air Solutions for Industry



- **ALZETA Corporation**
2343 Calle Del Mundo
Santa Clara, CA 95054
Alzeta.com
- **John Sullivan**
 - Sr. VP of Research & Development
 - 408-727-8282
 - jsullivan@alzeta.com